

Apparatus & Method for Reducing Nitrate Concentration in Wastewater

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This application is a continuation-in-part of U.S. application number 09/481,462 filed on January 11, 2000, and hereby claims the benefit thereof.

BACKGROUND OF THE INVENTION

Field of the Invention. This invention relates to the treatment of wastewater, namely a method for reducing nitrate concentration in wastewater.

Background. Wastewater is treated to remove its bacterial nutrients, principally biochemical oxygen demand (BOD). BOD is degraded by bacteria primarily by consuming dissolved oxygen (DO) to assist in metabolizing the BOD (aerobic metabolism). Oxygen is provided in treatment systems by aeration. In an oxygen depleted environment when DO levels in the wastewater are sufficiently reduced (anoxic environment), bacteria readily metabolize nitrates in the wastewater. Nitrate reduction by bacteria, however, is generally inefficient in the presence of oxygen. Bacteria capable of functioning in oxygen-rich and oxygen-poor environments will preferably metabolize nutrients aerobically.

If an anoxic environment is maintained for a sufficient time period, nitrate levels within the wastewater can be substantially reduced because bacteria will be forced to consume nitrates as a food source resulting in reduced nitrate concentrations in the effluent (outgoing water). This process is referred to as de-nitrification.

New environmental regulations are requiring reduction in nitrate levels in the effluent from wastewater treatment systems. Several methods, such as those disclosed in United States Patents 5,582,734 and 4,663,044 discuss possible solutions to nitrate removal in large municipal and commercial wastewater treatment plants. These

solutions are inapplicable to relatively small, self-contained wastewater treatment systems that are employed throughout the United States for treatment of wastewater. The small self-contained systems serve wastewater sources that include single family dwellings located in areas not served by municipal sewerage systems. Like larger commercial and municipal treatment systems, these smaller systems are becoming subjected to stricter nitrate removal regulations and encounter treatment problems when attempting to reduce nitrate levels in the wastewater. Unfortunately, no practical solution has been provided that will effectively solve the problems encountered by the small, self-contained systems.

ADVANTAGES AND OBJECTS OF THE INVENTION

The methods of the present invention provide a solution for small, self-contained wastewater treatment systems and work without interruption of flow into the systems. The present invention works with existing and new systems without additional substantial expense and effort and provides methods for effective nitrate reduction in the effluent from the small, self-contained systems.

With the aforementioned considerations in mind, it is therefore an object of this invention to provide a method for reducing nitrate levels in wastewater.

It is a further object of this invention to provide a safe and economical method of reducing nitrate concentration in wastewater that can be used with existing wastewater treatment systems.

It is a further object of the present invention to provide a method for reducing nitrate concentration in wastewater that can be implemented during a continuous wastewater flow situation.

It is a further object of the present invention to provide a method of reducing nitrate concentration in wastewater wherein the method is activated during periods of heavy diurnal flow.

It is a further object of the present invention to provide a method of reducing nitrate concentration in wastewater wherein the method is activated by a change in the dissolved oxygen level in the wastewater.

These and other advantages and objects of this invention shall become apparent from the ensuing description of the invention.

SUMMARY OF THE INVENTION

The present invention comprises apparatuses and method for reducing the nitrate concentrations in wastewater.

The present invention comprises a method for reducing nitrate concentration in wastewater in a wastewater treatment apparatus configured to define an aeration zone and a quiescent zone, wherein wastewater may continuously flow into the aeration zone. The wastewater treatment apparatus further comprises at least one gas outlet positioned within the aeration zone to provide gas flow into the aeration zone when wastewater is present in the aeration zone. The method comprises the step of ceasing gas flow into the aeration zone for a predetermined nitrate reduction period.

The present invention is also a method comprising the steps of ceasing gas flow into the aeration zone during periods of heavy flow and intermittently mixing the wastewater within the aeration zone.

The present invention also comprises a method for reducing the nitrate concentration in wastewater wherein the wastewater apparatus further comprises a dissolved oxygen monitor positioned to monitor the dissolved oxygen levels of the wastewater in the aeration zone. The method comprises the steps of: (a) monitoring the dissolved oxygen level in the aeration zone; (b) ceasing gas flow into the aeration zone when a predetermined dissolved oxygen level has been reached; and, (c) resuming gas flow into the aeration zone when a second predetermined threshold has been reached or a certain period of time has elapsed.

The present invention also comprises a method for reducing nitrate concentration in wastewater in a wastewater treatment apparatus wherein the method comprises the steps of: (a) monitoring the dissolved oxygen level in the aeration zone; (b) ceasing gas flow into the aeration zone when a predetermined dissolved oxygen level has been reached; and, (c) mixing the wastewater in the aeration zone.

The present invention also comprises a wastewater treatment apparatus configured to have an aeration zone and a quiescent zone. The apparatus comprises (a) at least one gas outlet positioned in the aeration zone and fluidly connected to a source of gas; (b) a dissolved oxygen probe positioned in the aeration zone; and, (c) a first controller adapted to regulate gas flow from the source of gas wherein the dissolved oxygen probe provides a dissolved oxygen measurement that is input to the first

controller. The present invention also comprises a wastewater treatment apparatus configured to define an aeration zone and a quiescent zone. The apparatus comprises (a) one or more gas outlets positioned in the aeration zone; (b) a timer adapted to regulate gas flow from a source of gas to the gas outlets; (c) a repeat cycle timer adapted to regulate gas flow from the source of gas to the gas outlets, whereby when the timer suspends gas flow into the gas outlets, the repeat cycle timer permits gas flow to the gas outlets at predetermined mixing intervals for predetermined mixing periods.

BRIEF DESCRIPTION OF THE DRAWINGS

Figure 1 illustrates a wastewater treatment apparatus that may be used with the methods of the present invention.

Figure 2 illustrates a wastewater treatment apparatus that has the wastewater inlet positioned near the bottom of the tank.

Figure 3 illustrates a wastewater treatment apparatus that includes a DO probe.

Figure 4a illustrates a schematic of an embodiment of the timer/repeat cycle timer control system.

Figure 4b illustrates a schematic of an embodiment of the programmed logic controller-DO input control system.

DETAILED DESCRIPTION OF

PREFERRED EMBODIMENTS OF THE INVENTION

Illustrations of construction, design, and methods of operation of the invention are set forth below with specific references to the Figures. However, the inventors do not intend to limit the scope of the invention to these embodiments.

During diurnal flow, the DO levels in aeration zone 1 are reduced because bacteria within the wastewater consumer oxygen in metabolizing the increased BOD levels of the influent wastewater. Because DO levels in the aeration chamber decrease during periods of heavy flow (and consequently high BOD), these heavy flow periods are ideal for nitrate removal because the amount of oxygen available for BOD metabolism is decreased. Consequently, bacteria gravitate toward nitrate metabolism. While the use of the present invention during diurnal flow is preferred, the methods may also be used outside of the periods of diurnal flow.

One method for reducing the nitrate concentration of wastewater in a wastewater treatment apparatus 3 is ceasing the gas (preferably air) flow into apparatus 3 for a predetermined nitrate reduction period during heavy flow intervals or when the DO level in the wastewater in aeration zone 1 reaches a first predetermined threshold, usually at or below about 2.0 mg/l. It is believed that a threshold level below 1.0mg/l is preferred. The predetermined nitrate reduction period can vary by apparatus, but predetermined nitrate reduction period preferably lasts between about 1 and about 2 hours (for a 500 gallon tank 4) or other time sufficient to substantially reduce the nitrate concentration of the wastewater.

The method for reducing nitrate concentration of wastewater may also include a mixing step to ensure that some of the particles that settle during the nitrate reduction period are re-suspended in aeration zone 1. Preferably, the wastewater in aeration zone 1 is mixed so that particles in the wastewater do not settle and are efficiently metabolized during the de-nitrification process. The efficiency of the present methods is

increased when the bacteria are circulated throughout aeration zone **1** to allow denitrification to occur throughout aeration zone **1** (as opposed to being concentrated at the bottom of tank **4**).

The mixing step can be performed in a variety of ways. In one embodiment, gas is intermittently flowed through gas outlets **29**, such as by (1) pulsing gas through at least one gas outlet **29** at predetermined mixing intervals and/or for predetermined mixing periods; (2) flowing a sufficient amount of gas through at least one gas outlet **29** at a sufficient flow rate to re-suspend most of the settled particles within the wastewater; and/or, (3) continuously flowing gas through at least one gas outlet **29** at a predetermined mixing interval for a predetermined mixing period.

Viewing Figure 4a, the pulsing or intermittent flow through gas outlets **29** can be accomplished using: (1) a clock timer **1005** or other means to control the start of the denitrification sequence (e.g., shutting off the gas (air) source or reducing the air supply); and, (2) a repeat cycle timer **1000** or other device to periodically pulse the air source for flow. Other “timing” devices could be substituted for the clock timer and repeat cycle timer; for instance, a timer could be used for the repeat cycle timer, and an internal clock of a processor, clock circuit, or PLC circuit could be used as a substitute for the clock timer or repeat cycle timer; alternatively, the timers could be a software embodied “virtual clock”; all such timing devices are considered as a timing means. The control system shown in Figure 4a comprises a repeat cycle timer **1000** and associated contacts **1001**, a clock timer **1005** and associated contacts **1006** and **1007**, a controller

1010 and associated contacts 1011, and a source of gas (air), preferably a compressor 1020.

When controller contacts 1011 are closed, power is provided to compressor 1020, and compressor 1020 flows air through gas outlets 29. Power is provided to controller 1010 when clock contact 1006 is closed (and consequently clock contact 1007 is open) or when clock contact 1006 is open. When clock contact 1006 is open, clock contact 1007 is closed, thereby providing power to repeat cycle timer 1000 to periodically (at the predetermined mixing intervals) close contact 1001 for specific periods of time (predetermined mixing periods). In turn, power is provided to controller 1010 and compressor 1020, thereby regulating flow through air drops 8 and gas outlets 29. Accordingly, both timer 1005 and repeat cycle timer 1010 are adapted to regulate the air flow from compressor 1020 to gas outlets 29 by controlling the power input to compressor 1020.

When apparatus 3 is configured to flow gas into aeration zone 1 at predetermined mixing intervals, the predetermined mixing intervals are sufficiently spaced so that suspended particles within the wastewater in aeration zone 1 do not settle, preferably between about 10 and about 20 minutes. At the beginning or end of each predetermined mixing interval, gas flows through at least one gas outlet 29 for a predetermined mixing period, preferably long enough to sufficiently mix the wastewater in aeration zone 1, but not long enough to substantially raise DO levels. Air for mixing can be supplied through one of the air outlets 29, or through a separate line. For a 500-gallon tank 4, a preferred predetermined mixing period is about 1 minute.

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In alternative embodiments, mixing can be provided by propellers within aeration zone 1, pumps, or other means to stir the wastewater in aeration zone 1. A simple means of stirring or mixing the wastewater step may be accomplished by suitably positioning wastewater inlet 6 so that the incoming flow of wastewater creates a current 5 (shown by the arrows in Figure 2) to accomplish the desired mixing.

A suitable embodiment is shown in Figure 2, where the inlet end 11 of wastewater inlet 6 is positioned near the bottom of tank 4. Inlet end 11 is positioned so that wastewater flowing from inlet end 11 does not pass into quiescent zone 2 through opening 9 until after it has been treated in aeration zone 1. When positioned near the bottom of tank 4, inlet end 11 should not be positioned so that incoming wastewater is directed toward opening 9. Placing inlet end 11 so that incoming wastewater flows tangentially to the walls of tank 4 prevents these problems. Alternatively, the mixing may be accomplished by combining some of the above means, such as placing inlet end 11 near the tank bottom and pulsing air into aeration zone 1 during the denitrification process.

Viewing Figure 3, apparatus 3 may further comprise a probe 21 that monitors and measures DO levels in aeration zone 1 and is in communication with a source of air (compressor 1020) using a valve, relay, solenoid or other suitable device to regulate or cease air flow through outlets 29. A suitable DO probe 21 is model TELL Fluoroprobe and Meter available from Tipton Environmental Inc. of Milford, Ohio. The air flow through air drops 8 ceases when probe 21 has detected a predetermined DO level or a predetermined change in DO level.

5 The predetermined change in DO levels may be a 10-20 percent change between measurements. Alternatively, the predetermined change in DO levels may be a 15 percent change over a running average of the measured DO levels for a twenty-minute period (the background level) when compared with the running average over a shorter period (e.g., 5 minutes).

Referring to Figure 4b, control of the process may be provided by a by a first controller **2001**, such as programmable logic controller (PLC) **2000**, and any included or associated memory storage devices. DO probe **21**, through DO meter **2040**, outputs a signal **2030** to PLC **2000**. PLC **2000** then operates compressor controller **2010** to close contact **2011** to operate a compressor **2020** to regulate the air flow from compressor **2020** by controlling the power supply to compressor **2020**. PLC **2000** may have associated memory to record DO measurements for using the measurements in calculations (e.g., determining background DO levels). PLC **2000** should also have an internal clock or associated with an external clock (not shown) so that PLC **2000** can pulse compressor controller **2010** as needed (and if desired) during de-nitrification, or simply power-up compressor controller **2010** after a predetermined time interval, such as the predetermined mixing interval.

Air flow through air drops **8** may resume when a second predetermined threshold is reached. Second predetermined threshold may comprise a time period, a subsequent DO level, or predetermined percent change between subsequent DO levels or a plurality of sequential DO levels. In terms of time, second predetermined threshold may equal the predetermined nitrate reduction period, approximately 1-2 hours. The

second predetermined threshold may also equal a subsequent DO measurement, about 1.0 mg/l or less, a subsequent predetermined percent change between subsequent DO measurements, or a subsequent predetermined percent change over a plurality of DO measurements. The second predetermined threshold is preferably the predetermined
5 nitrate reduction period because low DO level measurements may be erratic and/or unreliable.

The present methods may take a variety of combinations of the different steps described herein. For example, the present method may comprise ceasing gas flow for a predetermined nitrate reduction period. The present method may comprise ceasing
10 airflow into apparatus 3 and mixing the wastewater in aeration zone 1. The present method may comprise monitoring the DO levels, ceasing gas flow when a predetermined DO level has been reached, and resuming gas flow when a second predetermined threshold has been reached, with no mixing involved. Finally, the
15 method may comprise monitoring the DO levels, ceasing air flow into the aeration zone when the DO level has reached a first predetermined threshold, and mixing wastewater in aeration zone 1.

Unlike prior art methods, the present method may be used as wastewater continuously flows into apparatus 3 eliminating the necessity of ceasing flow into the wastewater treatment system during the nitrate reduction period. The embodiments
20 described herein are designed so that apparatus 3 may accept incoming wastewater without requiring sequential batch processing or storage of influent during denitrification.

Although the preferred embodiment has been described, it will be appreciated by those skilled in the art to that the present invention pertains that modifications, changes, and improvements may be made without departing from the spirit of the invention defined by the claims.

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